

(19)



Europäisches Patentamt

European Patent Office

Office européen des brevets



(11)

**EP 0 609 079 B1**

(12)

**EUROPEAN PATENT SPECIFICATION**

(45) Date of publication and mention  
of the grant of the patent:  
22.07.1998 Bulletin 1998/30

(51) Int. Cl.<sup>6</sup>: **B01J 8/22**, C10G 2/00,  
C07C 1/04

(21) Application number: **94300600.7**

(22) Date of filing: **27.01.1994**

**(54) Process for producing liquid and, optionally gaseous products from gaseous reactants**

Verfahren zur Herstellung von flüssigen und, gegebenenfalls von gasförmigen Produkte aus  
gasförmigen Reaktanten

Procédé pour la production de produits liquides et, éventuellement aussi gazeux, à partir de réactifs  
gazeux

(84) Designated Contracting States:  
**AT BE DE DK ES FR GB GR IE IT NL PT SE**

(30) Priority: **27.01.1993 ZA 930588**

(43) Date of publication of application:  
**03.08.1994 Bulletin 1994/31**

(73) Proprietor:  
**SASOL CHEMICAL INDUSTRIES  
(PROPRIETARY) LIMITED  
Johannesburg, Transvaal Province (ZA)**

(72) Inventors:  
• Jager, Berend  
Sasolburg, Orange Free State (ZA)  
• Steynberg, André Peter  
Vanderbijlpark, Transvaal Province (ZA)  
• Inga, Juan Ricardo  
Pittsburgh PA 15213 (US)

• Kelfkens, Renus Constantyn  
Secunda, Transvaal Province (ZA)  
• Smith, Michael Anthony  
Sasolburg, Orange Free State (ZA)  
• Malherbe Francois Erenst Johannes  
Sasolburg, Orange Free State (ZA)

(74) Representative:  
Barlow, Roy James  
J.A. KEMP & CO.  
14, South Square  
Gray's Inn  
London WC1R 5LX (GB)

(56) References cited:  
WO-A-93/16796                      FR-A- 873 645  
US-A- 2 540 706

• PATENT ABSTRACTS OF JAPAN vol. 9, no. 309  
(C-318)5 December 1985 & JP-A-60 147 228  
(MITSUBISHI JUKOGYO K.K.) 3 August 1985

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid. (Art. 99(1) European Patent Convention).

## Description

THIS INVENTION relates to a process for producing liquid and, optionally, gaseous products from gaseous reactants. It relates also to an installation for producing liquid and, optionally, gaseous products from gaseous reactants.

WO-A-93/16796 discloses a slurry reactor containing an internal filtering unit. A pressure differential exists across the filtering membrane and pressure fluctuations are imposed. The magnitude of the pressure fluctuations may be such, that some backflushing will occur.

According to a first aspect of the invention, there is provided, broadly, a process for producing liquid, according to claim 1.

While it is believed that the process can at least in principle have broader application, it is envisaged that the solid particles will normally be catalyst particles for catalyzing the reaction of the gaseous reactants into the liquid product, and, when applicable, the gaseous product; and the suspension liquid will normally, but not necessarily always, be the liquid product.

Furthermore, while it is also believed that, in principle, the process can have broader application, it is envisaged that it will have particular application in hydrocarbon synthesis where the gaseous reactants are capable of reacting catalytically in the slurry bed to form liquid hydrocarbon product and, optionally, gaseous hydrocarbon product. In particular, the hydrocarbon synthesis may be Fischer-Tropsch synthesis, with the gaseous reactants being in the form of a synthesis gas stream comprising mainly carbon monoxide and hydrogen, and with both liquid and gaseous hydrocarbon products being produced.

The catalyst particles can thus be any desired Fischer-Tropsch catalyst, such as an iron-based catalyst, a cobalt-based catalyst, or any other Fischer-Tropsch catalyst. The catalyst particles may have a desired particle size range, eg no particles greater than 300 microns and less than 5% by mass of the particles being smaller than 22 microns. The catalyst particle size range may be selected, bearing in mind the filtering medium. Conversely, the filtering medium may be selected bearing in mind the catalyst particle size range.

The slurry bed can thus be provided in a suitable vessel, with unreacted reactants and gaseous product being withdrawn from the vessel above the slurry bed, and the separated liquid product also being withdrawn from the vessel. The vessel will thus be maintained at normal elevated pressure and temperature conditions associated with Fischer-Tropsch synthesis, eg a predetermined operating pressure in the range 18 to 50 bar, and at a predetermined temperature in the range 160°C and 280°C, or even higher for the production of lower boiling point product.

The slurry bed may be characterized thereby that it, and in particular the filtration zone thereof, is not

mechanically mixed or agitated, eg not mechanically stirred. The catalyst particles in the slurry bed, and in particular in the filtration zone thereof, are thus maintained in suspension by the turbulence created by the synthesis gas stream passing through the slurry bed, ie bubbling through the bed. The gas velocity through the slurry bed is thus sufficiently high to maintain the slurry bed, and in particular the filtration zone thereof, in a state of turbulence or suspension. Thus, the superficial gas velocity through the filtration zone may be between 5 and 70 cm/s, typically between 15 and 55 cm/s, based on the filtration zone open cross-sectional area.

According to a second aspect of the invention, there is provided an installation for producing liquid according to claim 15.

The filtering medium may be part of a filter cartridge or element mounted in the vessel, and may be of a type which is of elongate form, with the filtering medium being of cylindrical form and enclosing a filtrate collecting zone, and with a filtrate outlet for withdrawing filtrate, ie liquid product, being provided at one end thereof.

While, in principle, the filtering medium can be any desired filtering medium having a desired opening size to prevent catalyst particles passing therethrough, it is preferably of a type with which permanent clogging or impregnation thereof with the catalyst particles does not occur. Thus, the filtering medium can be a mesh, porous material such as ceramic, perforated sheet, spiral wire wound, eg from wedge wire, or the like.

The filter elements may be located at the same or different levels within the filtration zone. Preferably a number of the filter elements are located close to the upper surface of the slurry bed, ie the filtration zone is provided close to the upper surface of the slurry bed.

The filter elements may be arranged in a plurality of banks, with each filter bank comprising a number of the filter elements.

In principle, the elements can be located at any desired inclination; however, they are preferably located vertically with their liquid product or filtrate outlets directed downwardly.

The passage of the liquid product through the filtering media may be effected by applying a pressure differential across the filtering media and any cake build-up thereon. Preferably this pressure differential may be up to 8 bar, and is typically in the region of about 4 bar. The pressure differential may be effected by withdrawing the liquid product into a rundown vessel which is at a lower pressure than the reactor vessel, with the filtrate outlets of the filter elements being connected to the rundown vessel by means of suitable liquid product conduits. The conduits may include a primary liquid product conduit leading from the filtrate outlet of each filter element; a secondary liquid product conduit into which the primary conduits of all the filter elements of the particular bank of filter elements tie; and a tertiary liquid product conduit leading to the rundown vessel, with the secondary conduits all tying into the tertiary conduit.

The flushing fluid may be process or non-process derived liquid and/or gas, eg some of the liquid and/or gaseous product.

The backflushing may, in general, be effected in pulse-like fashion. Thus, the backflushing may comprise an initial pulse of flushing liquid and/or gas, optimally followed by one or more further pulses of flushing liquid and/or gas. Each backflushing pulse may comprise initiating backflushing rapidly, ie commencing flow of flushing fluid rapidly; and backflushing the elements rapidly with a volume of the flushing fluid. This volume of flushing fluid may be relatively large, eg approximately equivalent to the internal volume of the filter elements. It can, however, be less than the internal volume of the filter elements, eg less than half their internal volume. When the volume of flushing fluid used during the initial pulse is relatively large, the volume of flushing fluid used during a second pulse may be less than that of the initial pulse, eg less than half the internal volume of the elements. However, when the volume of flushing fluid used during an initial pulse is relatively small as hereinbefore described, then the volume of flushing fluid during a further or second pulse may be similar to that of the initial pulse. The nature of any further pulses, when utilized, and the volume of the flushing fluid used during such pulses, may be similar to those of the second pulse hereinbefore described.

The pressure differential across the filtering media and filter cake during backflushing may be up to 10 bar depending on the degree of clogging or age of the filtering media, and is typically in the region of 5 bar.

The flushing fluid flow rate may be at least 6000  $\ell/h/m^2$  of filtering media. Thus, the flushing fluid flow rate may be between 6000  $\ell/h/m^2$  of filtering media when the pressure differential across the filtering media is about 5 bar, and between about 10000 and 12000  $\ell/h/m^2$  when the pressure differential is about 10 bar.

The waiting period during which no filtering or backflushing takes place, ie during which there is no liquid flow through the filtering media of the elements, to enhance subsequent filtration, may be between 15 and 60 minutes, or even longer, but is typically about 30 minutes.

The liquid product conduits and rundown vessel may conveniently form part of the backflushing means, with the rundown vessel then also constituting a flushing fluid vessel and the liquid product conduits constituting flushing fluid conduits; however, if desired, a separate flushing fluid vessel and flushing fluid conduit leading from the flushing fluid vessel to the secondary conduits, may be provided. The backflushing means may include at least one quick opening valve or the like, for effecting the backflushing pulses, in one of the flushing conduits; and pressurizing means for pressurizing the flushing fluid vessel. Thus, backflushing may be effected by pressurizing the flushing fluid vessel with the vessel containing some flushing liquid and/or gas, which may be product, and then actuating the quick

opening valve until the desired volume of flushing liquid and/or gas has passed through the filter elements of a bank of the filter elements in the second direction. Instead of utilizing a pressurized flushing fluid vessel, a pump and/or compressor can be used for supplying the flushing fluid to the filter elements.

In particular, backflushing may be effected by propelling or forcing residual liquid product in the conduits back through the filter elements in the second direction, preferably also through a restriction orifice located in the primary conduit of each filter element, by means of pressurized gas. It has been found that cleaning of the filter element surfaces is considerably improved, thus enhancing subsequent filtering performance thereof, when backflushing with the gas is effected for at least a sufficiently long period of time to displace substantially all the residual liquid product through the restriction orifices back into the filter elements. Backflushing with gas also has the advantage that the gas thereby introduced into the reactor vessel and which is removed with the product gas, does not have to be filtered again, thereby reducing loading on the filter elements during filtration.

The invention will now be described by way of example with reference to the accompanying diagrammatic drawings.

In the drawings,

FIGURE 1 shows a simplified flow diagram of a large pilot plant installation according to one embodiment of the invention, for producing gaseous and liquid products from gaseous reactants; FIGURE 2 shows an enlarged side view of one of the filter elements shown in Figure 1; FIGURE 3 shows, in part, an enlarged sectional view through III-III in Figure 2; FIGURE 4 shows, in part, a sectional view through IV-IV in Figure 2; and FIGURE 5 shows a simplified flow diagram of an installation according to another embodiment of the invention, for producing gaseous and liquid products from gaseous reactants.

Referring to Figures 1 to 4, reference numeral 10 generally indicates an installation according to one embodiment of the invention, for producing gaseous and liquid products from gaseous reactants.

The installation 10 includes an upright cylindrical Fischer-Tropsch synthesis reactor vessel 12.

The vessel 12 provides a slurry bed zone normally containing a slurry bed 14 of catalyst particles suspended in liquid product and through which gas is passing, as described in more detail hereunder. The slurry bed 14 has an upper surface 16, and the expanded height of the slurry bed 14 while gas passes through it is typically between 14 and 18 m when the total reactor length is about 24 m.

A synthesis gas flow line or conduit 18 is connected to a gas inlet (not shown) provided at the bottom of the

vessel 12, while a gas withdrawal flow line or conduit 20 leads from a gas outlet (not shown) provided at the top of the vessel 12. A suitable gas distributor (not shown) is connected to the gas inlet.

The installation 10 also includes a plurality of filter elements 30 (only some of which are shown) located in a filtration zone 22 within the slurry bed 14, arranged in a plurality of banks. Each filter element 30 is of elongate cylindrical form, and comprises a cylindrical filtering medium 32 enclosing a filtrate or liquid collecting zone 33. The medium 32 is located between end plates 34, 36, a mounting rod 38 protrudes from the end plate 34, while a flanged liquid outlet 40 is provided on the end plate 36. Thus, by means of the outlet 40, filtrate or liquid can be withdrawn from the collecting zone of the element or cartridge 30. The elements 30 are mounted in position in the vessel 12 by means of the rod 38 and flanged outlets 40. This mounting is not shown in detail in the drawings, but is typically effected by connecting the rod 38 to a lattice or grid spanning the vessel 12, while the outlet is connected to a conduit as hereinafter described.

The filtering medium 32 comprises a spiral wound wire 42 embedded in, or attached to, circumferentially spaced elongate supports 44 extending between the end plates 34, 36. Filtration openings or slots 46 are thus provided between adjacent loops of the wire 42. The wire 42 has, adjacent the openings or slots 46, surfaces 47 which taper away from each other, in the direction of the collecting zone. The wire 42 thus also has surfaces 48 against which a cake of catalyst particles (not shown) will form, as described in more detail hereunder, when liquid product is filtered by the elements 30 as it passes through the slots 46 in the direction of arrow 49. As a result of the tapering surfaces 47, solid particles will not readily permanently clog or impregnate the openings or slots 46 when filtered product passes through in the direction of arrow 49.

Typically, the filter elements 30 have an external diameter of 11 to 12 cm, with the wire 42 being of stainless steel. The wire 42 is typically about 1,2 mm wide at its base. The width of the slots or openings 46 is typically between 0,02-0,04 mm.

Instead of the filter elements 30, any other suitable elongate filter elements or cartridges, such as ceramic or sintered metal filter elements, can be used.

The filtration zone 22 is preferably located at a high level within the slurry bed, so that the filter elements 30 are located near the upper surface 16 thereof. As a result, they will not be embedded in settled solids or catalyst on slumping of the bed 14 which will occur if the gas feed to the vessel 12 is interrupted. However, it has been found that the filtration zone 22 need not necessarily be located near the top of the slurry bed 14 but can instead be located lower down since, should such bed slump occur, it has been found permanent clogging of the filter elements 30 will still not readily occur even if the elements are completely surrounded by settled sol-

ids or catalyst.

The elements 30 are preferably located with their outlets 40 directed downwardly so that any solid or catalyst fines which pass through the slots 46 with the filtrate (liquid product) will tend to collect in the bottom of the collection zones of the filter elements 30 from where they will be washed out with the liquid product.

To the outlet 40 of each of the filter elements 30 is connected a primary conduit 51, fitted with a restriction orifice 50. The conduits 51 of all the filter elements 30 making up a bank of the elements tie into a common secondary conduit 53 fitted with a shut-off valve 52. All the conduits 53 tie into a common tertiary conduit 54, fitted with a quick opening valve 56. A conduit 55 leads from the conduit 54 and is fitted with a shut-off or isolation valve 58. The conduit 55 leads into the top of a liquid blowdown vessel 60. A liquid rundown conduit 62, fitted with a shut-off valve 64, leads from the bottom of the vessel 60. The conduit 55 also serves as a back-flushing conduit for gas. Alternatively, a liquid backflush conduit 66, fitted with a shut-off valve 68, can lead from the conduit 62, upstream of the valve 64, back to the conduit 54, between the valves 56, 58.

A pressurizing gas conduit or line 70, fitted with a control valve 72 leads into the top of the vessel 60, while a vent conduit or line 74, fitted with a control valve 76, leads from the top of the vessel 60.

In use, synthesis gas, comprising mainly carbon monoxide and hydrogen, enters the reactor vessel 12 along the flow line 18. The gas flow rate to the vessel 12 is such as to give a superficial gas velocity in the filtration zone 22, based on the open cross-sectional area of the filtration zone, of between 5 and 70 cm/s, typically about 30 to 40 cm/s.

In the reactor vessel 12, which is characterized thereby that it contains no mechanical mixing or agitation device such as a mechanical stirrer, the slurry bed 14 is maintained. As mentioned above, the slurry bed 14 comprises catalyst particles suspended in liquid product, ie liquid wax produced in the vessel 12 on reaction of the gaseous reactants. The catalyst particles are maintained in suspended state in the slurry bed 14, and in particular in the filtration zone 22, only by means of the turbulence created therein by the gas passing upwardly therethrough. This turbulence also inhibits excessive cake build-up on the filtering media, and thus enhances filtration through the media.

The catalyst can be any suitable Fischer-Tropsch synthesis catalyst, and can typically be an iron-based catalyst prepared by precipitation and spray-drying. The catalyst particle size distribution is such typically that there are no particles larger than 300 microns, while the fraction of particles smaller than 22 microns is typically less than 5% by volume of the catalyst loaded into the reactor vessel 12. However, it has been found that while the proportion of small particles, ie particles smaller than 22 microns, should be as low as possible, up to 40% by volume of such particles, based on total catalyst

volume, can be tolerated. It has further been found that higher filtration rates are achievable when the content of particles smaller than 5 microns is minimized. However, it has been found that up to 25% by volume of such particles, based on total catalyst volume and measured in the end of run slurry, still gives satisfactory filtration rates. The mass percentage of catalyst in the catalyst/liquid product slurry of the slurry bed 14 is up to 40%.

The vessel 12 is typically maintained at an operating pressure of about 20 bar, and at an operating temperature between 180°C and 260°C, typically about 240°C. However, the operating pressure can be in excess of 20 bar, and the operating temperature higher or lower than 240°C, as hereinbefore described, depending on the nature and spread of gaseous and liquid products required and the type of catalyst used. Naturally, the vessel 12 will be provided with suitable temperature control means, such as cooling coils for controlling the reaction temperatures, as well as suitable pressure control means such as a pressure control valve.

In the vessel 12, as the synthesis gas passes through the slurry bed 14, the carbon monoxide and hydrogen react to form a range of products in accordance with known Fischer-Tropsch reactions. Some of these products are in gaseous form at the operating conditions of the vessel 12 and are withdrawn, together with unreacted synthesis gas, along the flow line 20. Some of the products produced, such as the waxes already mentioned, are in liquid form at the operating conditions of the vessel 12, and act as the suspension medium for the catalyst particles. As liquid product is formed, the level 16 of the slurry bed naturally rises, and the liquid product is thus withdrawn in the filtration zone by means of the filter elements 30 and rundown vessel 60 to maintain the slurry bed level. This internal filtration constitutes a first stage of the operating cycle of the filter elements 30.

The liquid product which passes through the filter elements 30 and which contains a relatively small concentration of solids (catalyst) typically between 2 and 200 ppm, passes, by means of the conduits 53, 54 and 55 into the vessel 60. The vessel 60 is maintained, by means of pressurizing gas introduced along the line 70, at elevated pressure, which is, however, lower than that in the vessel 12. Typically, the pressure in the vessel 60 is set such that the pressure differential across the filtering media of the elements 30 and any filter cake build-up thereon, is about 4 bar.

In this fashion, a relatively constant slurry bed level in the reactor is maintained. However, when the filter cake has built up to some thickness, it must then be backflushed from the filtering media, in a second stage of the operating cycle of the filter elements 30. The backflushing is effected by shutting the quick opening valve 56 and valve 58, and withdrawing at least some of the liquid product in the rundown vessel 60, through the

flow line 62, in order to remove any solids which have settled out in the bottom of the vessel 60. The pressure in the vessel 60 is then increased, by means of the gas pressurizing line 70, to a pressure greater than the operating pressure in the vessel 12. As a result of the static head of liquid (wax) in the rundown conduits, the liquid pressure at the quick opening valve 56 is typically slightly lower than the pressure in the vessel 60, but still sufficient for backflushing. When it is desired to backflush with liquid, the vessel 60 will thus contain some liquid product; however, if it is desired to backflush with gas, the vessel 60 will be pressurized with gas only, which can then be gaseous product such as tail gas.

Backflushing is effected in pulse-like fashion on one bank of filter elements 30 at a time, using either liquid product or gas. Thus, during backflushing, one of the valves 52 will be open, with the remaining valves 52 closed. For backflushing with liquid, valve 68 will be open, while for backflushing with gas, valve 58 will be open. In a first backflushing step, the quick opening valve 56 is opened rapidly in less than 0.8 seconds, and a volume of liquid product or gas, approximately equivalent to the internal volume of the filter elements 30 making up the bank of elements being flushed, is allowed to pass from the vessel 60, to produce a flow through the backflushing conduit 66 or 55, and the conduits 54, 53 and 51, thereby to provide flushing fluid through the bank of elements 30, in a second direction opposite to the direction in which the product flows during filtering. This typically takes up to 30 seconds. Thereafter, the quick opening valve 56 is again shut.

If a second backflushing step is desired, the vessel 60 is then again repressurized. In a second pulse-like backflushing step, the quick opening valve 56 is again opened rapidly for a second time. This time a flushing fluid volume equivalent to about one-third of the volume in the first backflushing operation, is allowed to pass from the vessel 60 to the filter elements 30. The valve 56 is thereafter again closed. If desired, at least one further similar backflushing step can be effected on that particular bank or filter elements.

Thereafter, the remaining banks of elements can similarly be backflushed, by opening and closing the appropriate valves 52.

In particular, rapid backflushing may be effected by using pressurized gas, which forces residual liquid product in the conduits through the filter elements in the second direction. Preferably, backflushing is then effected at least until backflushing gas starts passing through the restriction orifices. This leads to the advantages hereinbefore set out, viz effective cleaning of the filter element surfaces, and reducing extra loading of the filtering elements during filtration to no more than the volume of the residual liquid product in the conduits and filter elements, which is displaced during backflushing with the gas.

Without wishing to be bound thereby, it is believed that, during the first or initial backflushing step, any gas

which has collected in the elements 30, is displaced by the backflushing fluid and some dislodging of the filter cake from the filtering media may be effected. During the subsequent backflushing step, dislodging and breaking up of the filter cake from the media by hydraulic action is primarily effected.

The flow rate of flushing fluid, during the first and second backflushing steps, is typically between 6000 and 9000  $\text{l/h/m}^2$  of filtering medium at a pressure differential of about 5 bar, and between 10000 and 12000  $\text{l/h/m}^2$  of filtering media at a pressure differential of about 10 bar, as hereinbefore described. The flow and distribution of the flushing fluid to the filter elements 30 of the bank of elements being flushed, is regulated by means of the restriction orifices 50, which typically have orifice sizes of about 7,5 mm, but the actual size depends on the flow per element and the number of elements per bank. The restriction orifices 50 thus serve to distribute the backflushing fluid evenly between the filter elements 30 of the bank being flushed.

Thereafter, in a third stage of the operating cycle of each bank of filter elements 30, they are subjected to a waiting period in which no liquid passes through them. The Applicant has found that the filtration rate, when the filter elements 30 are then thereafter again subjected to filtration as hereinbefore described, increases with an increase in the duration of the waiting or non-active period. However, this must be balanced against the disadvantage that the filter elements are out of service during these waiting times. It has been found that a waiting period of between 15 and 30 minutes gives good results. It is believed that, during this waiting period, catalyst which has been loosened from the filter media of the elements 30 and partially broken up during the backflushing stage, is effectively broken up further, removed from the filter media surfaces and re-mixed remotely from the filters 30, by means of the turbulence within the slurry bed 14. It is believed further that the gas superficial velocity through the filtration zone 22 may influence the optimum duration of the waiting period.

During the waiting period, gas is vented from the rundown vessel 60 by means of the line 74, in order to return the vessel 60 to the pressure required for the subsequent filtering operation.

It is believed that, by means of the internal filtration and backflushing as hereinbefore described, the slurry bed 14 can be maintained at relatively constant levels for prolonged periods of continuous operation. In pilot and commercial plant tests which have been conducted, it was found that the vessel 12 could operate reliably for several months with no permanent clogging of the filter elements 30 or mechanical failure thereof occurring. It may, however, be necessary to withdraw some slurry from time to time, and to add fresh catalyst, eg to maintain catalyst activity.

During the tests, it was also found that good instantaneous filtration rates, on average in excess of 500

$\text{l/h/m}^2$ , were obtained, provided that the waiting period to which the filter elements were subjected was at least 15 minutes, and preferably about 30 minutes as hereinbefore described.

Referring to Figure 5, reference numeral 100 generally indicates an installation according to another embodiment of the invention, for producing gaseous and liquid products from gaseous reactants.

Parts of the installation 100 which are the same or similar to those of the installation 10 hereinbefore described with reference to Figures 1 to 4, are indicated with the same reference numerals.

In the installation 100, each conduit 53 is provided with one of the quick opening valves 56, while the pressurizing conduit 70 for the vessel 60, and the backflush conduit 66 are dispensed with. Instead, each of the conduits 53 is in the form of a loop, with the valve 56 provided near one end of the loops, and valves 102, 104, which are similar to the valves 52, 56 respectively, near another end of the loop. The conduits 53 also tie into a common backflush fluid conduit 106, which leads from a backflush fluid vessel 110, and is fitted with a valve 108. A gas pressurizing line 112, fitted with a valve 114, leads into the vessel 110, as does a backflush liquid feed line 116, fitted with a valve 118.

For liquid backflush, the vessel 110 is supplied, by means of the flow line 116, with backflush liquid which can be, but is not limited to, filtered wax from the vessel 60. The pressure in the vessel 110 is maintained at a pressure which is preferably at least 5 bar higher than the pressure in the reactor vessel 12 by means of gas introduced along the flow line 112. The rate at which gas is introduced is preferably sufficient to prevent a drop in pressure in the vessel 110 of more than 1 bar during backflushing.

For gas backflush, no liquid is supplied to the vessel 110 which is thus filled only with gas, eg tail gas, introduced along the flow line 112.

Backflushing is effected on one bank of filter elements 30 while maintaining filtration through the remaining banks, by closing the filtration valve 56 of that bank. This is followed by rapid opening, preferably in less than 1 second, of the backflush valve 104 of that bank of elements. The backflush valve 104 remains open for a period which is sufficient for the required volume of backflush fluid to flow out of the backflush vessel 110 along the conduit 106, and is thereafter closed. Once the pressure in the backflush vessel has been restored by means of gas, the backflushing can be repeated on the same filter bank, or on the next bank of element by opening and closing the required filtering valves 56, and opening the appropriate backflush valve 104.

If desired, instead of using the backflush vessel 110, a pump 120, fitted with a controlled kickback loop, for liquid backflush, or a compressor (not shown) for gas backflush, can be used, as indicated in broken line in Figure 5.



In known slurry bed reactors in which gas is subjected to catalytic reaction, separation of liquid product from catalyst particles is effected externally, ie some of the slurry is removed from the reactor vessel, and all or part of the liquid separated therefrom outside the reactor vessel, with the residue, which is then a dry catalyst or a slurry more concentrated in solids, returned to the reactor vessel. This separation can be by means of external hydrocyclones or magnetic separation devices. However, such an arrangement has the drawbacks of requiring a multiplicity of hydrocyclones with resultant multiplicity of pipes, valves and pumps, resulting in high capital costs. Furthermore, the separation is normally only partial, and hydrocyclones are prone to erosion so that high maintenance and operating costs arise.

Instead, the withdrawn slurry can be subjected to external decantation, ie the solids allowed to settle under quiescent conditions, and the resultant clarified liquid product decanted. However, such decantation is slow, requires large high pressure vessels which need to be operated isothermally to prevent remixing due to convection, separation is usually incomplete, pumps are required, capital costs are high, and a large catalyst inventory is required.

Yet further, external filtration equipment can be used. However, this is also capital intensive in view of the considerable piping and number of external vessels required. Furthermore, the slurry needs to be transferred to the filtration equipment by means of pumps, syphons or pressure drops, which affect catalyst quality negatively. The handling of slurries from the reactor to the filtration equipment, and of thick slurries from the filtration equipment back to the reactor, is cumbersome and requires substantial mechanical equipment, instrumentation and control equipment, which is capital intensive and also leads to high operating costs.

It is believed that the installations 10, 100 with the internal filtration, apart from having the advantages hereinbefore set out, also have the following advantages over the known external separating means as hereinbefore described, such as

- slurry and catalyst handling and transfer systems and equipment in the form of pipes, pumps and tanks are largely eliminated, since the filter cakes are formed on the filter elements inside the reactor and, on backflushing, are directly dispersed back into the slurry bed of the reactor;
- the re-slurrying of the filter cake, which requires some effort, is easily effected through the natural turbulence present in the slurry bed in the reactor, as a result of the gas bubbling through the slurry bed;
- the filter elements 30 and filter cakes are at all times kept at process conditions which, in the slurry bed 14, are practically isothermal;
- in the known reactors, should there be unplanned shut-downs, slurries and high melting point liquids

(waxes) in external filtration equipment can easily solidify on cooling, causing blockages; in the installations 10, 100 it is easier to keep the reactor vessel 12 at a sufficiently high temperature to prevent such cooling down, or to drain it, thereby substantially reducing the risk of blockages of filters;

- in the installations 10, 100, the catalyst inventory is kept to a minimum, ie catalyst costs are minimized, since backflushing of the internal filter elements 30 occurs frequently enough to prevent excessive build-up, and hence temporary "loss", of catalyst in the filter cake;
- the catalyst in the filter cakes in the installations 10, 100, and the liquid products, are always at the reactor process conditions, and there is thus reduced risk of deactivation of the catalyst and deterioration of the products, which can occur when external separation equipment is used and in which it is difficult to maintain these conditions;
- being able to minimize the period that liquid products are kept external to the reactor at the high temperature prevailing in the reactor 12 and which could otherwise lead to a deterioration of liquid product quality if subjected to these high temperatures for longer periods.

#### Claims

1. A process for producing liquid and, optionally, gaseous products from gaseous reactants, characterized in that the process comprises

feeding gaseous reactants at a low level into a slurry bed of solid particles suspended in a suspension liquid;  
 allowing the gaseous reactants to react as they pass upwardly through the slurry bed, thereby to form liquid and, optionally, gaseous products;  
 separating liquid product from the solid particles by passing, in a filtration zone within the slurry bed, liquid product through a filtration medium in a first direction, so that a cake of the solid particles forms on the filtration medium;  
 interrupting the passage of liquid product through the filtering medium;  
 backflushing the filtering medium by passing a flushing fluid through the filtering medium in a second direction, opposite to the first direction, for at least a portion of the period that the liquid product passage is interrupted, thereby to dislodge the cake from the filtering medium;  
 subjecting the filtering medium to a waiting period during which no filtering or backflushing therethrough takes place, to enhance removal of the filter cake as a result of turbulence within the slurry bed; and  
 again passing liquid hydrocarbon product

through the filtering medium in the first direction so that a cake of solid catalyst particles again forms on the filtering medium.

2. A process according to Claim 1, characterized in that the solid particles are catalyst particles for catalyzing the reaction of the gaseous reactants into the liquid product, and, when applicable, the gaseous product. 5
3. A process according to Claim 2, characterized in that the gaseous reactants are in the form of a synthesis gas stream comprising mainly carbon monoxide and hydrogen, with the gaseous reactants reacting in accordance with Fischer-Tropsch synthesis reactions, and with both liquid and gaseous hydrocarbon products being produced. 10
4. A process according to Claim 2 or Claim 3, characterized in that the slurry bed is provided in a reactor vessel, with unreacted reactants and any gaseous product being withdrawn from the vessel above the slurry bed, and the separated liquid product also being withdrawn from the vessel, the slurry bed being characterized thereby that at least its filtration zone is not mechanically mixed, with the catalyst particles in at least the filtration zone of the slurry bed thus being maintained in suspension by the turbulence created by the gaseous reactants passing through the slurry bed, and with the gas velocity through the slurry bed thus being sufficiently high to maintain at least the filtration zone of the slurry bed in a state of suspension. 15 20 25 30
5. A process according to Claim 4, characterized in that the superficial gas velocity of gasses passing through the filtration zone is between 5 and 70 cm/s, based on the filtration zone open cross-sectional area. 35 40
6. A process according to Claim 4 or Claim 5, characterized in that a plurality of the filtering media, arranged in banks, are provided, each filtering medium being provided by an elongate filter element mounted in the vessel and comprising the filtering medium which is in cylindrical form and a filtrate outlet for withdrawing liquid product at one end thereof, with the passage of the liquid product through the filtering elements being effected by applying a pressure differential of up to 8 bar across the filtering media of the elements and any cake build-up thereon. 45 50
7. A process according to Claim 6, characterized in that the pressure differential is effected by withdrawing the liquid product into a rundown vessel which is at a lower pressure than the reactor vessel, with the filtrate outlets of the filter elements being 55

connected to the rundown vessel by means of liquid product conduits, with the flushing fluid being liquid product and/or gaseous product, and with the backflushing including urging the flushing fluid through the conduits and filter elements in a direction opposite to the direction of normal liquid product flow during filtration.

8. A process according to Claim 7, characterized in that the backflushing is effected in pulse-like fashion, with an initial pulse of flushing liquid product and/or gaseous product, followed by at least one further pulse of flushing liquid product and/or gaseous product. 10
9. A process according to Claim 8, characterized in that each backflushing pulse comprises initiating flow of flushing fluid rapidly; and backflushing the elements rapidly with a volume of the flushing fluid. 15
10. A process according to claim 9, characterized in that the backflushing includes, during the initial pulse, forcing residual liquid product in the liquid product conduits through the filter elements in the second direction, by means of pressurized gaseous product. 20
11. A process according to claim 10 characterized in that, during the initial backflushing pulse, the residual liquid product is forced through a restriction orifice in the conduit below each filter element. 25
12. A process according to any one of claims 7 to 11 inclusive, characterized in that the pressure differential across the filtering media and any filter cake build-up thereon during backflushing is up to 10 bar depending on the properties of the filter cake. 30
13. A process according to any one of claims 7 to 12 inclusive, characterized in that the waiting period is between 15 and 60 minutes. 35
14. A process according to any one of the preceding claims, characterized in that the backflushing of the filtering medium is effected by passing a flushing liquid through the filtering medium. 40 45
15. An installation for producing liquid and, optionally, gaseous products from gaseous reactants, characterized in that the installation comprises 50

a reactor vessel having a slurry bed zone which, in use, will contain a slurry bed of solid particles suspended in a suspension liquid;  
a gas inlet in the vessel at a low level within the slurry bed zone, for introducing gaseous reactants into the vessel;  
a gas outlet in the vessel above the slurry bed



zone, for withdrawing unreacted gaseous reactants and, when present, gaseous products from the vessel;

a plurality of filter elements mounted in a filtration zone located within the slurry bed zone, each filtering element providing a filtering medium;

liquid displacement means for displacing liquid product through the filtering medium in a first direction, while solid particles build up as a cake on the filtering medium; and

backflushing means for passing a flushing fluid through the filtering medium in a second direction, opposite to the first direction, from time to time, thereby to dislodge the cake from the filtering medium.

16. An installation according to Claim 15, characterized in that the filter elements are of elongate form, with the filtering medium being of cylindrical form and enclosing a filtrate collecting zone, and with a filtrate outlet for withdrawing liquid product, being provided at one end thereof.

17. An installation according to Claim 16, characterized in that the filter elements are located vertically with their filtrate outlets directed downwardly, and are arranged in a plurality of banks each comprising a number of the filter elements.

18. An installation according to Claim 17, characterized in that it includes a primary conduit leading from the filtrate outlet of each filter element, a secondary conduit into which the primary conduits of all the filter elements of one of the banks of filter elements tie, and a tertiary conduit into which all the secondary conduits tie and which leads to a rundown vessel.

19. An installation according to Claim 18, characterized in that the liquid product conduits and rundown vessel form part of the backflushing means, with the rundown vessel then also constituting a flushing fluid vessel and the liquid product conduits also constituting flushing fluid conduits.

20. An installation according to Claim 18, characterized in that it includes a flushing fluid vessel and a flushing fluid conduit leading from the flushing fluid vessel to the secondary conduits.

21. An installation according to Claim 19 or Claim 20, characterized in that the backflushing means includes at least one quick opening valve for effecting backflushing in pulse-like fashion, in one of the flushing fluid conduits; and pressurizing means for pressurizing the flushing fluid vessel so that backflushing is effected by pressurizing the flushing fluid

vessel, with the vessel containing some flushing fluid, and then actuating the quick opening valve until the desired volume of flushing fluid gas has passed through the filter elements of one of the banks of the filter elements in the second direction.

22. An installation according to any one of Claims 18 to 21 inclusive, characterized in that the backflushing means includes a restriction orifice in the primary conduit of each filter element.

#### Patentansprüche

1. Ein Verfahren zur Herstellung flüssiger und wahlweise gasförmiger Produkte aus gasförmigen Reaktanden, dadurch gekennzeichnet, daß das Verfahren einschließt

die Einleitung gasförmiger Reaktanden an einer tiefliegenden Stelle in ein Aufschlammungsbett aus festen, in einer Suspensionsflüssigkeit suspendierten Partikeln;

die den gasförmigen Reaktanden gebotene Möglichkeit zu reagieren, während sie durch das Aufschlammungsbett nach oben steigen und dabei flüssige und wahlweise gasförmige Produkte bilden;

die Abtrennung von flüssigem Produkt von den festen Partikeln, indem das flüssige Produkt in einer Filtrationszone innerhalb des Aufschlammungsbettes in einer ersten Richtung ein Filtermedium passiert, so daß auf dem Filtermedium aus den festen Partikeln ein Kuchen gebildet wird;

die Unterbrechung der Passage von flüssigem Produkt durch das Filtermedium;

das Spülen des Filtermediums, indem ein Spülfluid das Filtermedium in einer zweiten, gegenüber der ersten entgegengesetzten Richtung passiert für mindestens einen Teil des Zeitraums, in dem die Passage des flüssigen Produktes unterbrochen ist, und der Kuchen dabei vom Filtermedium abgelöst wird;

eine dem Filtermedium verordnete Wartezeit, während der keine Filtration oder Spülung dort hindurch stattfindet, um das Entfernen des Filterkuchens infolge der Turbulenz innerhalb des Aufschlammungsbettes zu verbessern; und die erneute Passage von flüssigem Kohlenwasserstoffprodukt durch das Filtermedium in der ersten Richtung, so daß auf dem Filtermedium wiederum ein Kuchen aus festen Katalysatorpartikeln gebildet wird.

2. Ein Verfahren nach Anspruch 1, dadurch gekennzeichnet, daß die festen Partikel Katalysatorpartikeln zur Katalyse der Reaktion der gasförmigen Reaktanden zum flüssigen Produkt und, wenn

zutreffend, zum gasförmigen Produkt sind.

3. Ein Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß die gasförmigen Reaktanden in Form eines Stroms aus Synthesegas vorliegen, das in der Hauptsache aus Kohlenmonoxid und Wasserstoff besteht, und die gasförmigen Reaktanden gemäß dem Fischer-Tropsch-Verfahren miteinander reagieren, wobei sowohl flüssige als auch gasförmige Kohlenwasserstoffe gebildet werden. 5
4. Ein Verfahren nach Anspruch 2 oder 3, dadurch gekennzeichnet, daß das Aufschlämmbett in einem Reaktionsgefäß vorliegt, wobei nicht umgesetzte Reaktanden und gasförmige Produkte aus dem Gefäß oberhalb des Aufschlämmbettes abgezogen werden, und das abgetrennte flüssige Produkt ebenfalls aus dem Gefäß abgezogen wird, das Aufschlämmbett sich dadurch auszeichnet, daß zumindest seine Filtrationszone nicht mechanisch durchmischt wird, die Katalysatorteilchen zumindest in der Filtrationszone des Aufschlämmbettes auf diese Weise in Suspension gehalten werden aufgrund der Turbulenz, die durch die gasförmigen Reaktanden bei der Passage durch das Aufschlämmbett erzeugt wird, und die Gasgeschwindigkeit im Aufschlämmbett somit ausreichend hoch ist, um zumindest die Filtrationszone des Aufschlämmbettes im Zustand einer Suspension zu halten. 10 15 20 25 30
5. Ein Verfahren nach Anspruch 4, dadurch gekennzeichnet, daß die an der Oberfläche herrschende Gasgeschwindigkeit der die Filtrationszone passierenden Gase zwischen 5 und 70 cm/sek. beträgt, bezogen auf die offene Querschnittsfläche der Filtrationszone. 35
6. Ein Verfahren nach Anspruch 4 oder Anspruch 5, dadurch gekennzeichnet, daß eine Vielzahl von in Reihen angeordneten Filtermedien zur Verfügung stehen, wobei jedes Filtermedium durch ein längliches, im Gefäß montiertes Filterelement bereitgehalten wird, welches das in zylindrischer Form vorliegende Filtermedium enthält und an einem Ende einen Filtratablauf für das Abziehen von flüssigem Produkt aufweist und die Passage des flüssigen Produktes durch die Filterelemente unter Anwendung eines Druckunterschieds von bis zu 8 bar über den Filtermedien der Elemente und darauf gebildeten Kuchen erfolgt. 40 45 50
7. Ein Verfahren nach Anspruch 6, dadurch gekennzeichnet, daß der Druckunterschied durch Abziehen des flüssigen Produktes in eine Vorlage erzielt wird, die unter einem im Vergleich zum Reaktionsgefäß niedrigeren Druck steht, wobei die Filtratab-

läufe der Filterelemente mit Hilfe von Flüssigproduktleitungen mit der Vorlage verbunden sind, das Spülfluid ein flüssiges und/oder gasförmiges Produkt ist und die Spülung einschließt, und das Spülfluid in einer Richtung durch die Leitungen und Filterelemente gedrückt wird, die entgegengesetzt zu der des normalen Flüssigproduktstroms während der Filtration ist.

8. Ein Verfahren nach Anspruch 7, dadurch gekennzeichnet, daß die Spülung pulsierend erfolgt mit einem Initialimpuls des flüssigen und/oder gasförmigen Spülmittels, gefolgt von mindestens einem weiteren Impuls des flüssigen und/oder gasförmigen Spülmittels. 10
9. Ein Verfahren nach Anspruch 8, dadurch gekennzeichnet, daß jeder Spülimpuls ein schnelles Initialisieren des Spülfluidstroms und eine schnelle Spülung der Elemente mit einem Teil des Spülfluids beinhaltet. 15
10. Ein Verfahren nach Anspruch 9, dadurch gekennzeichnet, daß die Spülung während des Initialimpulses das Drücken von restlichem flüssigen Produkt in den Flüssigproduktleitungen durch die Filterelemente in der zweiten Richtung mit Hilfe von unter Druck stehendem gasförmigen Produkt einschließt. 20 25
11. Ein Verfahren nach Anspruch 10, dadurch gekennzeichnet, daß während des anfänglichen Spülimpulses das restliche flüssige Produkt durch eine Drosselungsöffnung in die Leitung unter jedem Filterelement gedrückt wird. 30
12. Ein Verfahren nach einem der Ansprüche 7 bis einschließlich 11, dadurch gekennzeichnet, daß der Druckunterschied quer durch die Filtermedien und einen darauf gebildeten Filterkuchen während des Spülens in Abhängigkeit von den Eigenschaften des Filterkuchens bis zu 10 bar beträgt. 35
13. Ein Verfahren nach einem der Ansprüche 7 bis einschließlich 12, dadurch gekennzeichnet, daß die Wartezeit zwischen 15 und 60 Minuten beträgt. 40 45
14. Ein Verfahren nach irgendeinem der vorstehenden Ansprüche, dadurch gekennzeichnet, daß die Spülung des Filtermediums durch Durchleiten einer Spülflüssigkeit durch das Filtermedium erfolgt. 50
15. Eine Anlage zur Herstellung flüssiger und wahlweise gasförmiger Produkte aus gasförmigen Reaktanden, dadurch gekennzeichnet, daß die Anlage

ein Reaktionsgefäß, das über eine Zone mit

- einem Aufschlammungsbett verfügt, die während des Betriebs ein Aufschlammungsbett aus festen Partikeln enthält, die in einer Suspensionsflüssigkeit suspendiert sind;  
 einen Gaseinlaß am Gefäß an einer tiefliegenden Stelle innerhalb der Zone des Aufschlammungsbettes für die Einleitung gasförmiger Reaktanden in das Gefäß;  
 eine Gasaustrittsöffnung am Gefäß oberhalb der Aufschlammungsschichtzone für das Abziehen von nicht umgesetzten gasförmigen Reaktanden und, wenn vorhanden, gasförmiger Produkte aus dem Gefäß;  
 eine Vielzahl von Filterelementen, die in einer Filtrationszone innerhalb der Aufschlammungsbettzone montiert sind, wobei jedes Filterelement ein Filtermedium bereithält;  
 Flüssigkeitsverdrängungsmittel zur Verdrängung von flüssigem Produkt durch das Filtermedium in einer ersten Richtung, während feste Partikel auf dem Filtermedium einen Kuchen bilden; und  
 Spülmittel zum zeitweiligen Durchfluß eines Spülfluids durch das Filtermedium in einer zweiten zur ersten entgegengesetzten Richtung, um dadurch den Kuchen vom Filtermedium abzulösen.
16. Eine Anlage nach Anspruch 15, dadurch gekennzeichnet, daß die Filterelemente in länglicher Form vorliegen, wobei das Filtermedium eine zylindrischer Form aufweist und eine das Filtrat sammelnde Zone einschließt, und an einem Ende einen Filtratablauf zum Abziehen von flüssigem Produkt aufweisen.
17. Eine Anlage nach Anspruch 16, dadurch gekennzeichnet, daß die Filterelemente mit ihren nach unten gerichteten Filtratabläufen senkrecht und in mehreren Reihen angeordnet sind, die jeweils eine Anzahl Filterelemente enthalten.
18. Eine Anlage nach Anspruch 17, dadurch gekennzeichnet, daß sie eine Primärleitung einschließt, die vom Filtratablauf jedes Filterelements führt, und eine zweite Leitung, in welche die Primärleitungen aller Filterelemente einer der Filterelementreihen münden, sowie eine dritte Leitung, in die alle Sekundärleitungen münden, die dann in eine Vorlage führt.
19. Eine Anlage nach Anspruch 18, dadurch gekennzeichnet, daß die Flüssigproduktleitungen und die Vorlage Teile der Spüleinrichtung sind, wobei die Vorlage dann auch ein Spülfluidgefäß darstellt und die Flüssigproduktleitungen auch Spülfluidleitungen sind.

20. Eine Anlage nach Anspruch 18, dadurch gekennzeichnet, daß sie ein Spülfluidgefäß und eine Spülfluidleitung einschließt, die vom Spülfluidgefäß in die Sekundärleitungen führt.
21. Eine Anlage nach Anspruch 19 oder 20, dadurch gekennzeichnet, daß die Spüleinrichtung mindestens ein Schnellöffnungsventil in einer der Spülfluidleitungen zur Durchführung der impulsweise erfolgenden Spülung einschließt, sowie eine Druckaufbauvorrichtung für das Unterdrucksetzen des Spülfluidgefäßes, so daß die Spülung dadurch erfolgt, daß man das Spülfluidgefäß unter Druck setzt, wobei das Gefäß etwas Spülfluid enthält, und anschließend das Schnellöffnungsventil betätigt, bis das gewünschte Volumen Spülfluidgas die Filterelemente von einer der Filterelementreihen in Gegenrichtung passiert hat.
22. Anlage nach einem der Ansprüche 18 bis einschließlich 21, dadurch gekennzeichnet, daß die Spüleinrichtung eine Drosselungsöffnung in der Primärleitung von jedem Filterelement einschließt.

## Revendications

1. Procédé pour produire des produits liquides et, de manière facultative, des produits gazeux à partir de réactifs gazeux, caractérisé en ce que le procédé comprend :

l'alimentation en réactifs gazeux à un niveau inférieur dans un lit de boue liquide de particules solides en suspension dans un liquide de suspension ;

l'autorisation pour que ces réactifs gazeux réagissent lorsqu'ils passent vers le haut à travers le lit de boue liquide, pour former ainsi des produits liquides et, de manière facultative, des produits gazeux ;

la séparation du produit liquide des particules solides en passant, dans une zone de filtration à l'intérieur du lit de boue liquide, le produit liquide à travers un milieu de filtration dans un premier sens, de sorte qu'une croûte des particules solides se forme sur le milieu de filtration ;

l'interruption du passage du produit liquide à travers le milieu de filtrage ;

le rinçage à contre courant du milieu de filtrage en passant un fluide de rinçage à travers le milieu de filtrage dans un second sens, opposé au premier sens, pour au moins une partie de la période pendant laquelle le passage du produit liquide est interrompu, pour déloger de ce fait la croûte du milieu de filtrage ;

la soumission du milieu de filtrage à une période d'attente pendant laquelle aucun fil-

- trage ou aucun rinçage à contre courant à travers ce dernier n'a lieu, pour améliorer l'enlèvement de la croûte de filtrage en conséquence d'une turbulence à l'intérieur du lit de boue liquide ; et  
5 le passage renouvelé du produit d'hydrocarbure liquide à travers le milieu de filtrage dans le premier sens de sorte qu'une croûte de particules solides de catalyseur se forme de nouveau sur le milieu de filtrage.
2. Procédé selon la revendication 1, caractérisé en ce que les particules solides sont des particules de catalyseur pour catalyser la réaction des réactifs gazeux dans le produit liquide, et, quand on peut l'appliquer, le produit gazeux.
3. Procédé selon la revendication 2, caractérisé en ce que les réactifs gazeux sont sous la forme d'un flot de gaz de synthèse comprenant principalement du monoxyde de carbone et de l'hydrogène, les réactifs gazeux réagissant selon des réactions de synthèse de Fischer-Tropsch, et des produits d'hydrocarbure liquides et gazeux étant tout deux produits.
4. Procédé selon la revendication 2 ou la revendication 3, caractérisé en ce que le lit de boue liquide est disposé dans une cuve de réacteur, les réactifs n'ayant pas réagi et tout produit gazeux étant extraits de la cuve au-dessus du lit de boue liquide, et le produit liquide séparé étant également extrait à partir de la cuve, le lit de boue liquide étant caractérisé, de ce fait, en ce qu'au moins sa zone de filtration n'est pas mélangée de façon mécanique, les particules de catalyseur dans au moins la zone de filtration du lit de boue liquide étant ainsi maintenues en suspension par la turbulence créée par les réactifs gazeux passant à travers le lit de boue liquide, et la vitesse du gaz à travers le lit de boue liquide étant ainsi suffisamment élevée pour maintenir au moins la zone de filtration du lit de boue liquide dans un état de suspension.
5. Procédé selon la revendication 4, caractérisé en ce que la vitesse superficielle du gaz passant à travers la zone de filtration est comprise entre 5 et 70 cm/s, sur la base de la surface en coupe transversale ouverte de la zone de filtration.
6. Procédé selon la revendication 4 ou la revendication 5, caractérisé en ce qu'une pluralité des milieux de filtrage, agencés en rangées, sont prévus, chaque milieu de filtrage étant muni d'un élément de filtrage allongé monté dans la cuve et comprenant le milieu de filtrage qui a une forme cylindrique et une sortie de produits filtrés pour extraire le produit liquide au niveau d'une extrémité particulière de ce
- dernier, le passage du produit liquide à travers les éléments de filtrage étant effectué en appliquant un différentiel de pression allant jusqu'à 8 bars de part et d'autre des milieux de filtrage des éléments et de toute croûte accumulée sur ces derniers.
7. Procédé selon la revendication 6, caractérisé en ce que le différentiel de pression est réalisé en extrayant le produit liquide dans une cuve de récupération qui est à une pression inférieure à la cuve de réacteur, les orifices de produits filtrés des éléments de filtrage étant reliés à la cuve de récupération au moyen de conduites de produit liquide, le fluide de rinçage étant un produit liquide et/ou un produit gazeux, et le rinçage à contre courant comprenant la poussée du fluide de rinçage à travers les conduites et les éléments de filtrage dans un sens opposé au sens de l'écoulement normal du produit liquide pendant la filtration.
8. Procédé selon la revendication 7, caractérisé en ce que le rinçage à contre courant est effectué à la manière d'une impulsion, avec une impulsion initiale de produit liquide et/ou de produit gazeux de rinçage, suivi par au moins une impulsion supplémentaire de produit liquide et/ou de produit gazeux de rinçage.
9. Procédé selon la revendication 8, caractérisé en ce que chaque impulsion de rinçage à contre courant comprend l'amorçage rapide de l'écoulement du fluide de rinçage; et le rinçage rapide à contre courant des éléments rapidement avec un certain volume du fluide de rinçage.
10. Procédé selon la revendication 9, caractérisé en ce que le rinçage à contre courant comprend, pendant l'impulsion initiale, la poussée du produit liquide résiduel dans les conduites de produit liquide à travers les éléments de filtrage dans le second sens, au moyen d'un produit gazeux pressurisé.
11. Procédé selon la revendication 10 et caractérisé en ce que, pendant l'impulsion initiale de rinçage à contre courant, le produit liquide résiduel est poussé à travers un orifice de limitation dans la conduite au-dessous de chaque élément de filtre.
12. Procédé selon l'une quelconque des revendications 7 à 11 incluses, caractérisé en ce que le différentiel de pression de part et d'autre des milieux de filtrage et d'une quelconque croûte de filtrage accumulée sur ces derniers pendant le rinçage à contre courant peut aller jusqu'à 10 bars en fonction des propriétés de la croûte de filtrage.
13. Procédé selon l'une quelconque des revendications 7 à 12 incluses, caractérisé en ce que la période

d'attente est comprise entre 15 et 60 minutes.

14. Procédé selon l'une quelconque des revendications précédentes, caractérisé en ce que le rinçage à contre courant des milieux de filtrage est effectué en passant un liquide de rinçage à travers les milieux de filtrage.

15. Installation pour produire des produits liquides et, de manière facultative, des produits gazeux à partir de réactifs gazeux, caractérisée en ce que l'installation comprend :

une cuve de réacteur ayant une zone de lit de boue liquide qui, en fonctionnement, va contenir un lit de boue liquide de particules solides en suspension dans un liquide de suspension ; une entrée de gaz dans la cuve à un niveau inférieur à l'intérieur de la zone de lit de boue liquide, pour introduire des réactifs gazeux dans la cuve ; une sortie de gaz dans la cuve au-dessus de la zone de lit de boue liquide, pour extraire, à partir de la cuve, des réactifs gazeux n'ayant pas réagi et, quand il y en a, des produits gazeux ; une pluralité d'éléments de filtrage montés dans une zone de filtration située à l'intérieur de la zone de lit de boue liquide, chaque élément de filtrage réalisant un milieu de filtrage ; des moyens de déplacement de liquide pour déplacer un produit liquide à travers le milieu de filtrage dans un premier sens, tandis que des particules solides s'accumulent comme une croûte sur le milieu de filtrage ; et des moyens de rinçage à contre courant pour passer un fluide de rinçage à travers le milieu de filtrage dans un second sens, opposé au premier sens, de temps en temps, pour déloger de ce fait la croûte du milieu de filtrage.

16. Installation selon la revendication 15, caractérisée en ce que les éléments de filtrage sont de forme allongée, le milieu de filtrage étant de forme cylindrique et entourant une zone de recueillement de produits filtrés, et une sortie de produits filtrés, pour extraire un produit liquide, étant prévue au niveau d'une extrémité particulière de ce dernier.

17. Installation selon la revendication 16, caractérisée en ce que les éléments de filtrage sont positionnés verticalement, leurs sorties de produits filtrés étant dirigées vers le bas, et sont agencés en une pluralité de rangées, chacune comprenant un certain nombre des éléments de filtrage.

18. Installation selon la revendication 17, caractérisée en ce qu'elle comporte une conduite primaire cheminant à partir de la sortie de produits filtrés de

chaque élément de filtrage, une conduite secondaire dans laquelle les conduites primaires de tous les éléments de filtrage d'un des bancs des éléments de filtrage sont fixées, et une conduite tertiaire dans laquelle toutes les conduites secondaires sont fixées et qui conduit à une cuve de récupération.

19. Installation selon la revendication 18, caractérisée en ce que les conduites de produit liquide et la cuve de récupération forment une partie des moyens de rinçage à contre courant, la cuve de récupération constituant alors également une cuve de fluide de rinçage et les conduites de produit liquide constituant également des conduites de fluide de rinçage.

20. Installation selon la revendication 18, caractérisée en ce qu'elle comprend une cuve de fluide de rinçage et une conduite de fluide de rinçage cheminant depuis la cuve de fluide de rinçage jusqu'aux conduites secondaires.

21. Installation selon la revendication 19 ou la revendication 20, caractérisée en ce que les moyens de rinçage à contre courant comportent au moins une vanne à ouverture rapide pour effectuer un rinçage à contre courant à la manière d'une impulsion, dans une des conduites de fluide de rinçage ; et des moyens de pressurisation pour pressuriser la cuve de fluide de rinçage de sorte qu'un rinçage à contre courant est effectué en pressurant la cuve de fluide de rinçage, la cuve contenant une certaine quantité de fluide de rinçage, et ensuite en actionnant la vanne à ouverture rapide jusqu'à ce que le volume souhaité de fluide de rinçage soit passé à travers les éléments de filtrage d'une des rangées des éléments de filtrage dans le second sens.

22. Installation selon l'une quelconque des revendications 18 à 21 incluses, caractérisée en ce que les moyens de rinçage à contre courant comprennent un orifice de limitation dans la conduite primaire de chaque élément de filtrage.

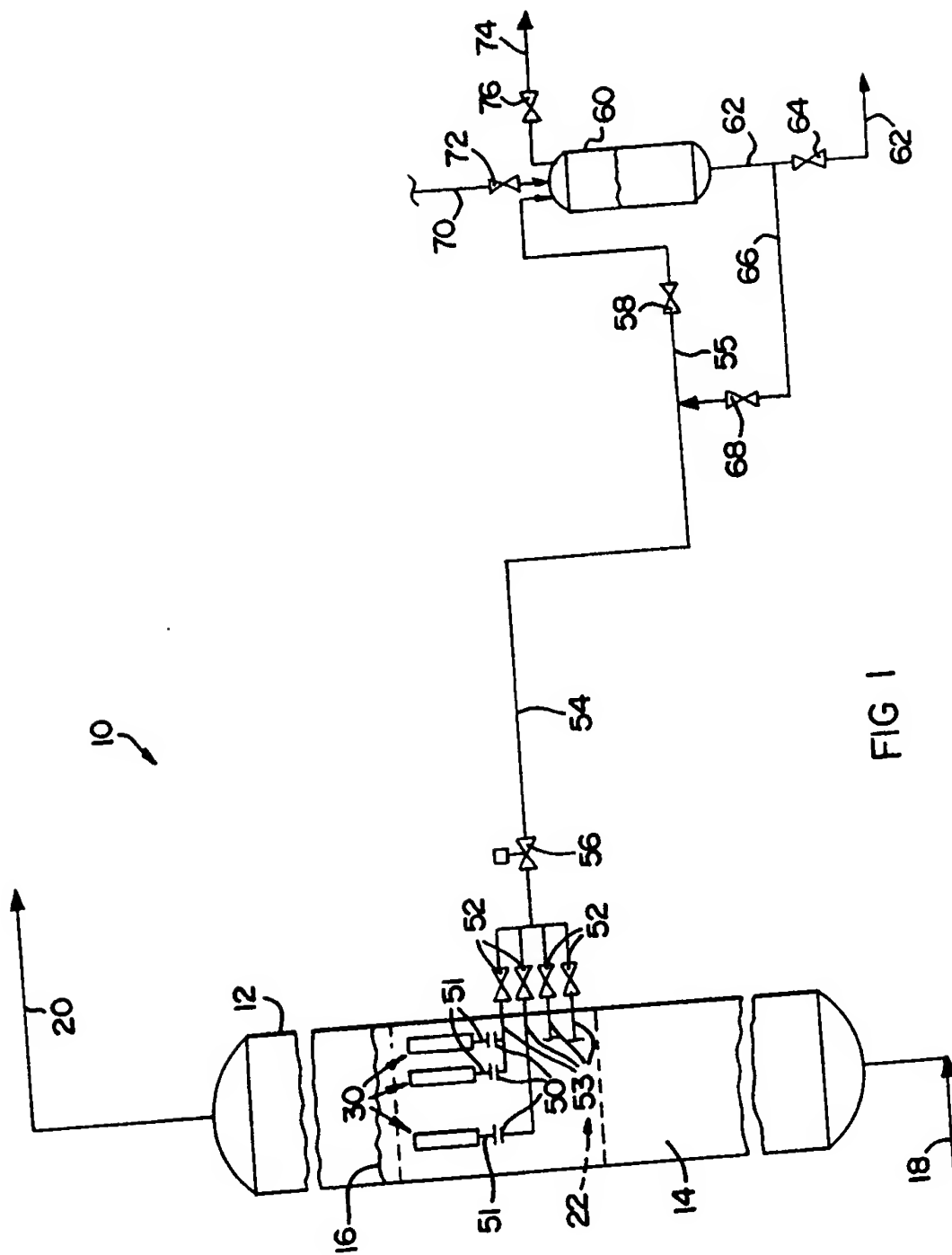


FIG 1



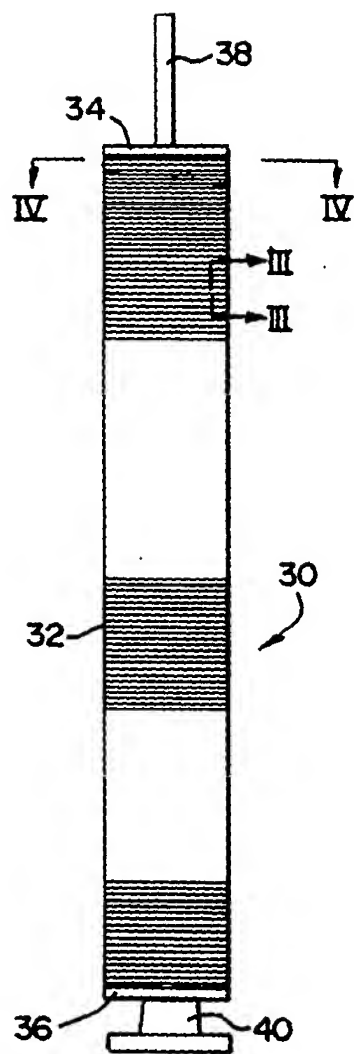


FIG 2

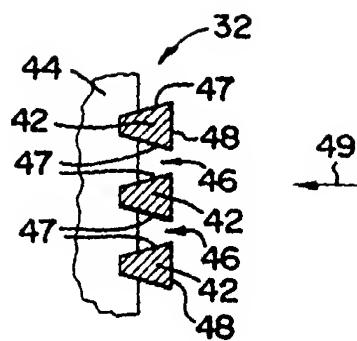


FIG 3

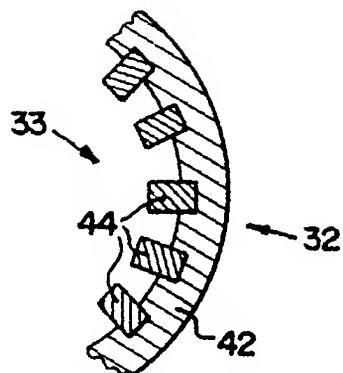
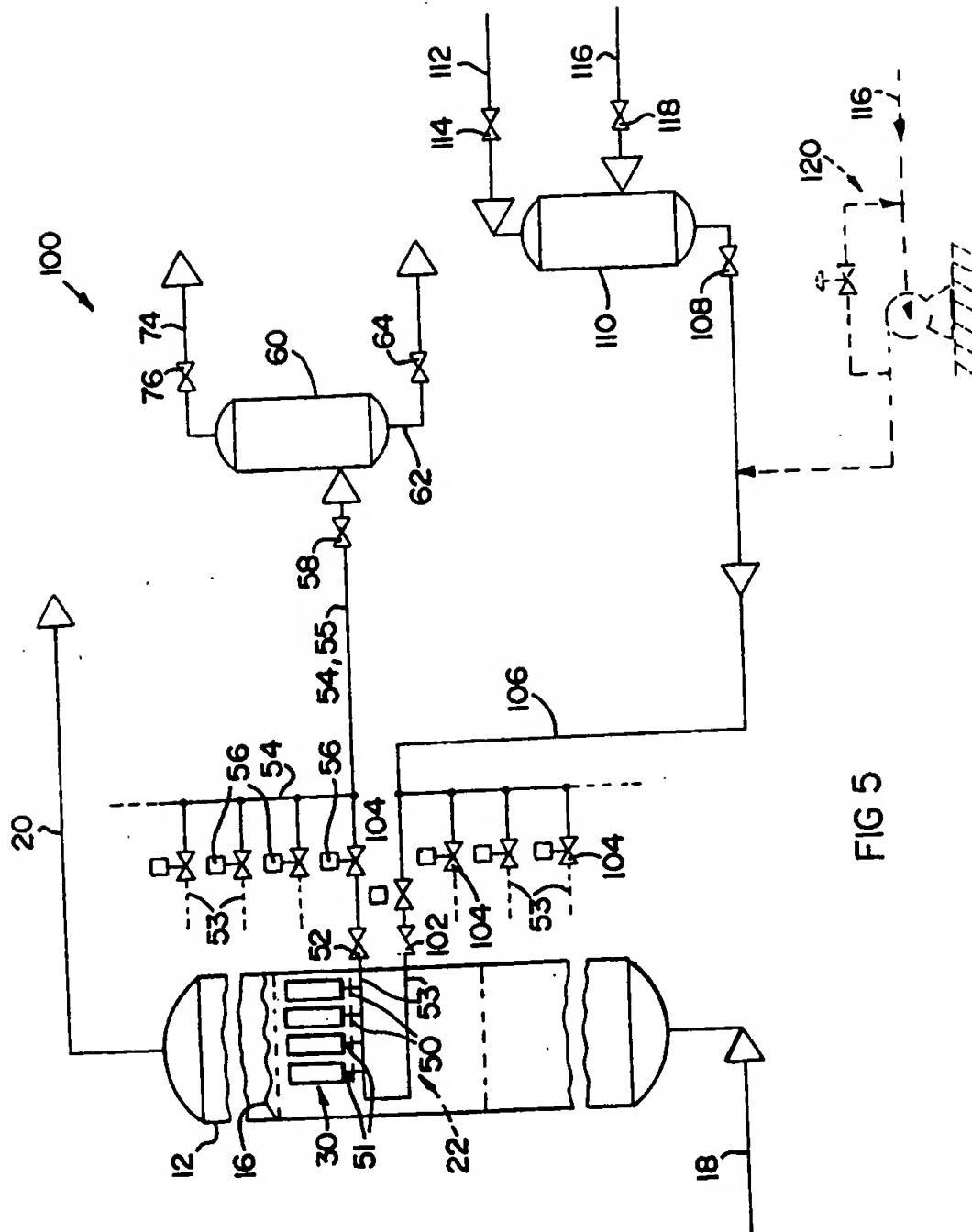


FIG 4



5615